

# Catalytic reduction of N<sub>2</sub>O with CH<sub>4</sub> over various Cu-SBA-15 catalysts

M.H.M. Husin<sup>1,2,\*</sup>, M.R. Nordin<sup>3</sup>, I.S. Mohamad<sup>1</sup>, S.Y. Chin<sup>4</sup>

<sup>1)</sup> Faculty of Mechanical Engineering, Universiti Teknikal Malaysia Melaka,  
Hang Tuah Jaya, 76100, Durian Tunggal, Melaka, Malaysia.

<sup>2)</sup> Centre for Advanced Research on Energy, Universiti Teknikal Malaysia Melaka,  
Hang Tuah Jaya, 76100, Durian Tunggal, Melaka, Malaysia.

<sup>3)</sup> Faculty of Technology Management & Technopreneurship, Universiti Teknikal Malaysia Melaka,  
Hang Tuah Jaya, 76100, Durian Tunggal, Melaka, Malaysia.

<sup>4)</sup> Faculty of Chemical and Natural Resources Engineering, Universiti Malaysia Pahang, Kuantan, 26300, Malaysia.

\*Corresponding e-mail: haizal@utem.edu.my

**Keywords:** N<sub>2</sub>O reduction; Cu-SBA-15 catalysts; N<sub>2</sub>O:CH<sub>4</sub> ratio

**ABSTRACT** – The N<sub>2</sub>O catalytic reduction by methane over Cu-SBA-15 molar ratio (1:30) was studied based on physical mixture, impregnation method and pH adjustment method preparation. All catalytic reduction of N<sub>2</sub>O with methane were carried out in a flow reactor system at atmospheric pressure with 100 mL/min total flow was used. For the N<sub>2</sub>O:CH<sub>4</sub> ratio effect, suggested that N<sub>2</sub>O reacts with CH<sub>4</sub> is represented by  $4\text{N}_2\text{O} + \text{CH}_4 \rightarrow 4\text{N}_2 + \text{CO}_2 + 2\text{H}_2\text{O}$ . The Cu/SBA-15 prepared by pH adjustment method has highest activity compared to Cu-SBA-15 prepared by impregnation method and physical mixture of CuO and SBA-15.

## 1. INTRODUCTION

Due to the increasing concern over environmental issues, studies on N<sub>2</sub>O have oriented towards the development of catalytic systems for its elimination. Various types of catalysts have been reported to be active for the decomposition of nitrous oxide. Cu-SBA-15 is one of those materials showing better prospects for application as catalyst for N<sub>2</sub>O decomposition [1-2]. Catalytic reduction is an alternative to catalytic decomposition with the potential to lower the temperature for effective N<sub>2</sub>O removal by addition of a reducing agent. Therefore, the use of hydrocarbons as reducing agent is widely and easily available, such as CH<sub>4</sub>, C<sub>3</sub>H<sub>6</sub> or C<sub>3</sub>H<sub>8</sub> required to meet commercial feasibility [3]. Previous report, the Cu/SBA-15 samples prepared by pH adjustment method shows higher activity on N<sub>2</sub>O decomposition due to copper atom was substituted in the framework of the SBA-15 with better dispersion of copper species on mesoporous silica and easily reduced copper-silica support interaction CuO to Cu due to the weakening of copper - silica support interaction [2,4]. Known that, CH<sub>4</sub> is strong greenhouse-effect gases with a global warming potential (GWP) per molecule of about 20 times that of carbon dioxide. Therefore, it is interesting studies that a selective catalytic reduction (SCR) of N<sub>2</sub>O by CH<sub>4</sub> is applied to simultaneous removal of N<sub>2</sub>O and CH<sub>4</sub> in the emission gases by various Cu-SBA-15.

## 2. METHODOLOGY

### 2.1 Cu on SBA-15 preparation

For Cu on SBA-15 molar ratio (1:30) by the pH adjustment and impregnation samples was prepared

based on previous report [2]. Meanwhile, physical mixture of copper oxide in SBA-15 samples was prepared by the required amount of powder form copper oxide was mixed together in one (1) gram of prepared SBA-15 to obtain Si:M molar ratios of 30:1.

### 2.2 N<sub>2</sub>O decomposition and reduction with CH<sub>4</sub>

The catalytic experiments were carried out in an alumina tube (4.76 mm i.d.) micro-reactor. Amount of 500.0 mg sample was filled into the tube to form a catalyst bed. The reaction temperature was monitored by a K-type thermocouple inserted inside the catalyst bed. The reaction unit was equipped with mass flow controllers and product analysis was performed with on-line gas chromatograph 7680A (Agilent) equipped with two columns in series (molecular sieve 5A and Heyasep Q) and TCD detector. For N<sub>2</sub>O decomposition, the reaction gas composed of 1.0% N<sub>2</sub>O in He at a total flow rate of 100 mL/min. Meanwhile for N<sub>2</sub>O reduction with CH<sub>4</sub>, reaction gas mixture was composed of 1.0 % N<sub>2</sub>O and 0.1%, 0.25% and 1% CH<sub>4</sub> in He at a total flow rate of 100 mL/min, respectively to N<sub>2</sub>O:CH<sub>4</sub> ratio of 10:1, 4:1 and 1:1.

## 3. RESULTS AND DISCUSSION

### 3.1 Effect of different N<sub>2</sub>O:CH<sub>4</sub> ratio

The effect of catalytic activity in the differences N<sub>2</sub>O:CH<sub>4</sub> volume ratio on N<sub>2</sub>O reduction reaction on Cu/SBA-15 (1:30) prepared by pH adjustment sample have been done. Figure 1 shows catalytic activity of N<sub>2</sub>O reduction by CH<sub>4</sub> at different N<sub>2</sub>O:CH<sub>4</sub> ratio compared to N<sub>2</sub>O decomposition in the absence of CH<sub>4</sub>. The catalytic activity of N<sub>2</sub>O decomposition on Cu/SBA-15 catalyst was significantly promoted by the presence of CH<sub>4</sub>. The conversions of CH<sub>4</sub> in different N<sub>2</sub>O:CH<sub>4</sub> volume ratio reactions were compared in Figure 2, CH<sub>4</sub> conversion increased with the reaction temperature and with N<sub>2</sub>O:CH<sub>4</sub> ratio. Meanwhile, Figure 3 shows the plotting graph N<sub>2</sub> and O<sub>2</sub> formation verses N<sub>2</sub>O conversion at different N<sub>2</sub>O:CH<sub>4</sub> ratio. The slope of the N<sub>2</sub>O decomposition to CH<sub>4</sub> conversion is 4.0, 1.0 and 0.33, for N<sub>2</sub>O:CH<sub>4</sub> ratio of 1:1, 4:1 and 10:1 respectively. Based on relationship of volume and mole of gases in Avogadro Law, suggested that N<sub>2</sub>O reacts with CH<sub>4</sub> is represented by  $4\text{N}_2\text{O} + \text{CH}_4 \rightarrow 4\text{N}_2 + \text{CO}_2 + 2\text{H}_2\text{O}$ . Simultaneous presence of N<sub>2</sub>O with CH<sub>4</sub> is essential for the high

selective catalytic reduction (SCR) activity of  $N_2O$  with  $CH_4$ . This is related to the high initial rate of  $CH_4$  in  $N_2O + CH_4$  reaction on Cu/SBA-15. The  $CH_4$  plays an important role in the  $N_2O$  reduction, because the catalytic activities in  $N_2O$  conversion were drastically enhanced by the presence of  $CH_4$ . According to Nobukawa and Sugawara, nascent oxygen transients ( $O^*$ ) from  $N_2O$  dissociation before accommodation on stable adsorption sites can play an important role in activation and oxidation of  $CH_4$ . Thus, it seems that methane effectively reduced oxidized active sites ( $O^*$ ) and therefore increased the rate of the  $N_2O$  conversion [5].

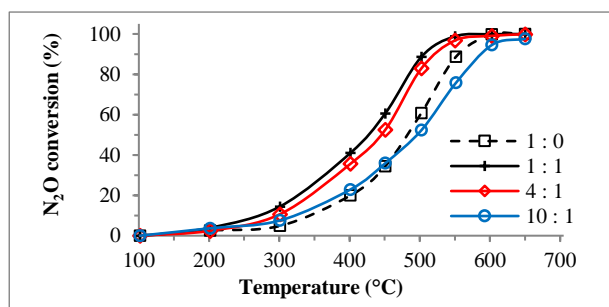


Figure 1 The catalytic activity of  $N_2O$  reduction by  $CH_4$  on Cu/SBA-15 at different  $N_2O:CH_4$  ratio.

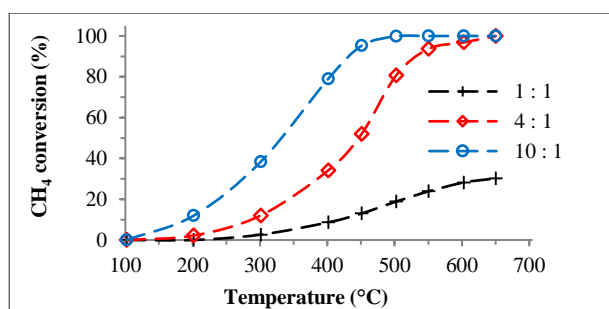


Figure 2  $CH_4$  conversion against Reaction temperature on different  $N_2O:CH_4$  ratio.

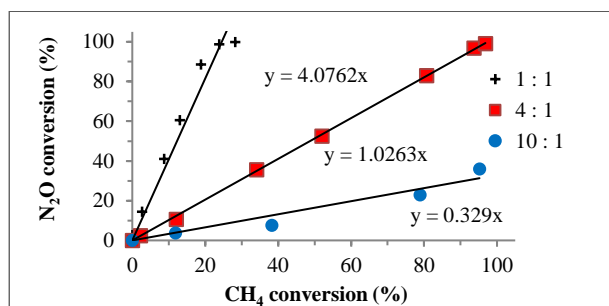


Figure 3 Plotting  $N_2O$  conversion versus  $CH_4$  conversion on different  $N_2O:CH_4$  ratio.

### 3.2. Catalytic activity of $N_2O$ conversion

Figure 4 present  $N_2O$  decomposition on various copper on SBA-15. Cu/SBA-15 prepared through pH modification sample highest activity causing 80 % conversion at 550 °C. Cu on SBA-15 prepared by impregnation method and physical mixture samples show reached 80 % conversion at 650 °C.

Meanwhile, catalytic activity of  $N_2O$  reduction by  $CH_4$  on various copper on SBA-15 was shows as in Figure 5. For Cu-SBA-15 impregnated, and CuO-SBA-15 physical mixture sample, the  $N_2O$  conversion curve

was shifted to the left from SBA-15 pure sample. Both catalysts sample reached 100% conversion of  $N_2O$  at 600°C. Meanwhile, Cu/SBA-15 pH adjustment sample was much higher than other samples  $N_2O$  reduction by  $CH_4$ .

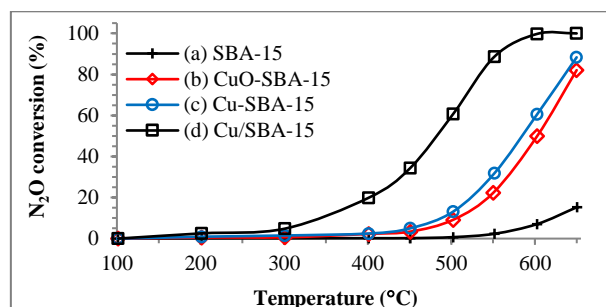


Figure 4 The catalytic activity of  $N_2O$  decomposition on (a) SBA-15, (b) CuO-SBA-15 (1:30) physical mixture, (c) Cu-SBA-15 (1:30) prepared by impregnated, and (d) Cu/SBA-15(1:30) prepared by pH modification.

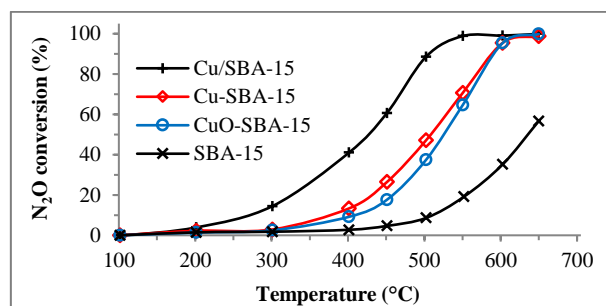


Figure 5 The catalytic activity of  $N_2O$  reduction by  $CH_4$  at  $N_2O:CH_4$  (1:1) volume ratio on various copper condition of (a) Cu/SBA-15 pH adjustment, (b) Cu-SBA-15 impregnated, (c), CuO-SBA-15 physical mixture and (d) SBA-15.

## 4. CONCLUSIONS

This paper has successfully demonstrated that the Cu/SBA-15 prepared by pH adjustment has highest activity compared to Cu-SBA-15 prepared by impregnation method and to physical mixture of CuO. Suggestion that  $N_2O$  reacts with  $CH_4$  in this study is represented by  $4N_2O + CH_4 \rightarrow 4N_2 + CO_2 + 2H_2O$ .

## ACKNOWLEDGMENTS

The authors would like to thank to Universiti Teknikal Melaka Malaysia for SLAB scholarship and study leave.

## REFERENCES

- [1] Chmielarz, L., Kuśtrowski, P., Kruszc, M., Dziembaj, R., Cool, P., & Vansant, E. F. (2005). Nitrous oxide reduction with ammonia and methane over mesoporous silica materials modified with transition metal oxides. *Journal of Porous Materials*, 12(3), 183-191.
- [2] Husin, M. H. M., Dewayanto, N., Li, J., & Nordin, M. R. (2015). The characteristics of copper containing SBA-15 prepared by impregnation and pH adjustment methods and their activities for [N. sub. 2] O decomposition. *Advances in Environmental Biology*, 9(6 S1), 6-15.

- [3] Fierro, G., Dragone, R., & Ferraris, G. (2008). NO and N<sub>2</sub>O decomposition and their reduction by hydrocarbons over Fe–Zn manganite spinels. *Applied Catalysis B: Environmental*, 78(1-2), 183-191.
- [4] Nordin, M. R., Husin, M. M. H., Li, J. L., Liew, K. Y., & Chin, S. Y. (2012). Copper containing SBA15 prepared through pH modification methods and its catalytic activity for N<sub>2</sub>O decomposition. *Journal of South-Central University for Nationalities (Natural Science Edition)*, 31(1), 1-7.
- [5] Nobukawa, T., Sugawara, K., Okumura, K., Tomishige, K., & Kunimori, K. (2007). Role of active oxygen transients in selective catalytic reduction of N<sub>2</sub>O with CH<sub>4</sub> over Fe-zeolite catalysts. *Applied Catalysis B: Environmental*, 70(1-4), 342-352.